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Monetary vs. RSV Reality



It's all about the Nameplate ...

Would a plant by any other size or type cost just as much?

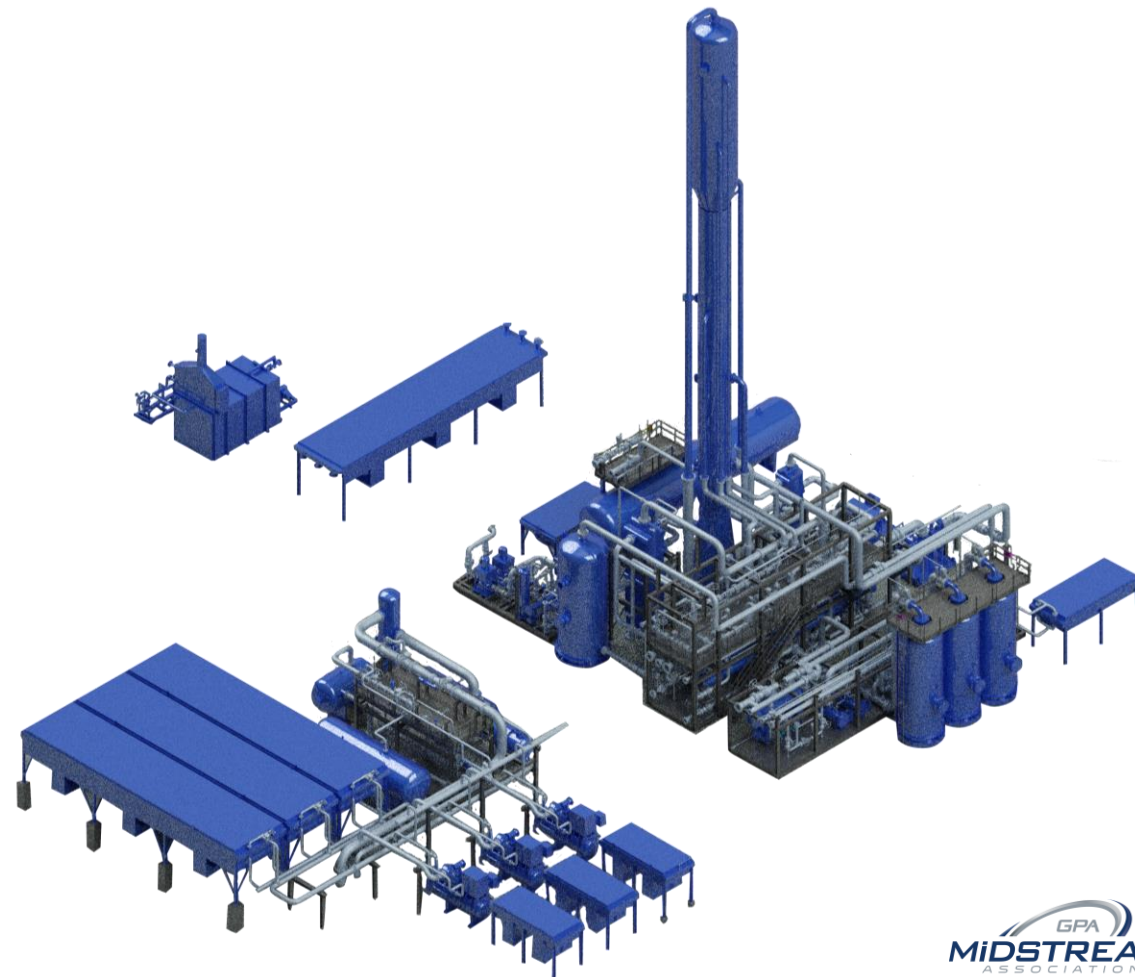
200MM

230MM

250MM

300MM

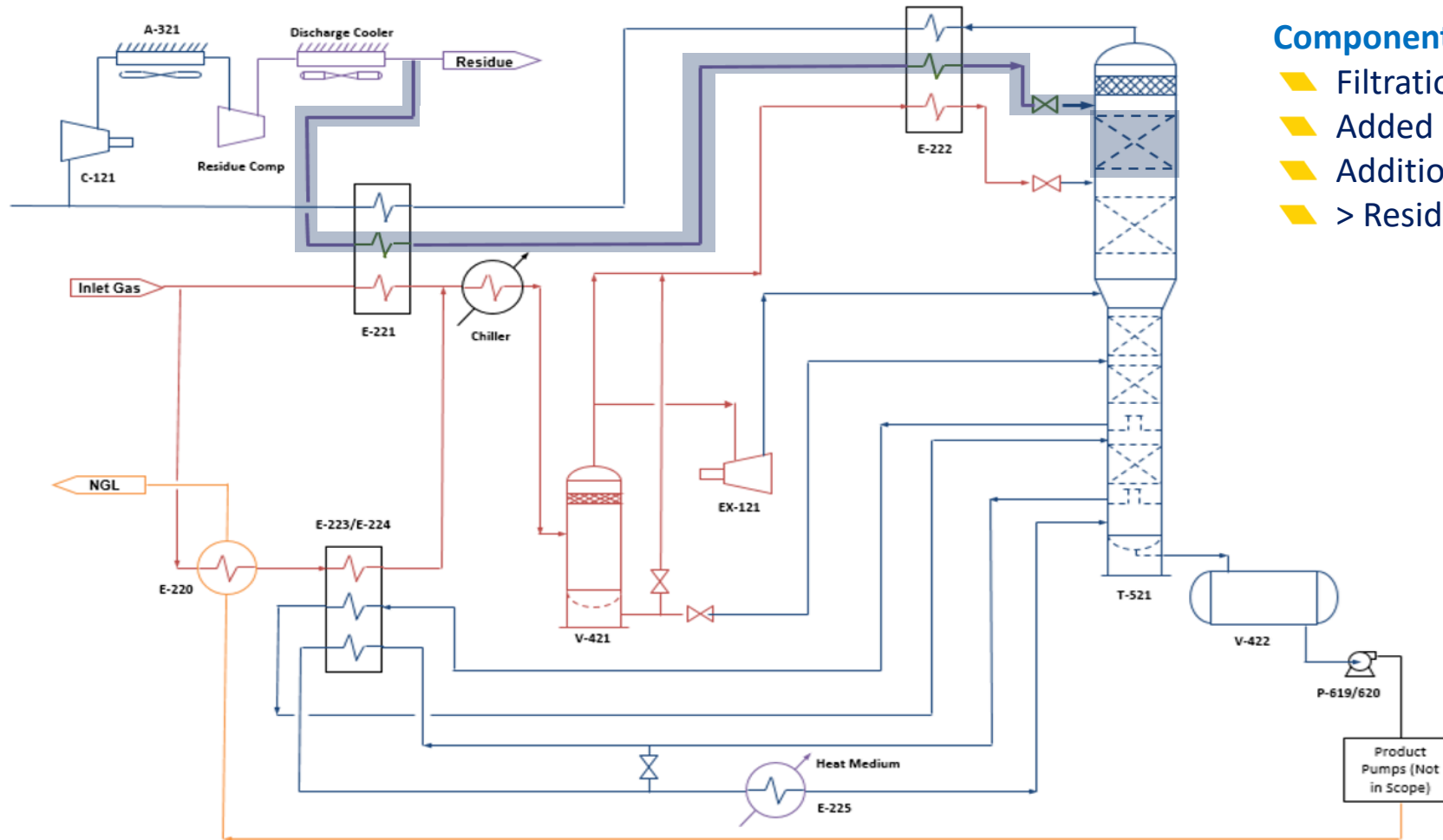
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What Matters Most? ...the Size

- Nameplate: 200 MMscfd has been extremely popular.
- However, the market trends upward with capacity – and the current mega facilities are pinched on plot and process >1 BCFD.
 - Site permitting and pre-planning for electrical expansion can hinder the facility's total processing capacity.
- Limited added **plant** capex is required to shift to 25% or even 50% greater nameplate. (CAPEX ↑ 10% to 30%).
 - Requires very limited added plot space.
- Fixed Fee Contract (stable for processors), @ \$0.65/Mscf
 - @ 200MMscfd, \$47.1 million
 - @ 250MMscfd, \$58.9 million
 - @ 230MMscfd, \$54.2 million
 - @ 300MMscfd, \$70.7 million
 - Scale-up 6/10ths rule applies: Turnkey CAPEX ROI of <2.5 years vs. 200 MM.
- Facility planning should address current market sizes and potential expansion to maximize profitability.
 - Balance of the plant should be updated or flexible.

What is Recycle Split Vapor?



Components

-  Filtration
-  Added BAHX Pass
-  Additional Tower Bed / Height
-  > Residue HP, added machine

E-220 Product Heater E-221 Gas/Gas E-222 Reflux Condenser E-223/E-224 Side/BTM Reboilers E-225 Trim Reboiler T-521 Demethanizer P-619/620 NGL Booster Pumps EX-121/C-121 Expander/Booster Comp V-421 Cold Separator V-422 NGL Surge Tank A-321 B. Comp Cooler

RSV Features

Added Recycle Reflux

- Cold separator temperatures ↑ and tower pressures ↑
- ≥ recoveries versus GSP even at richer gases

CO₂ Tolerance

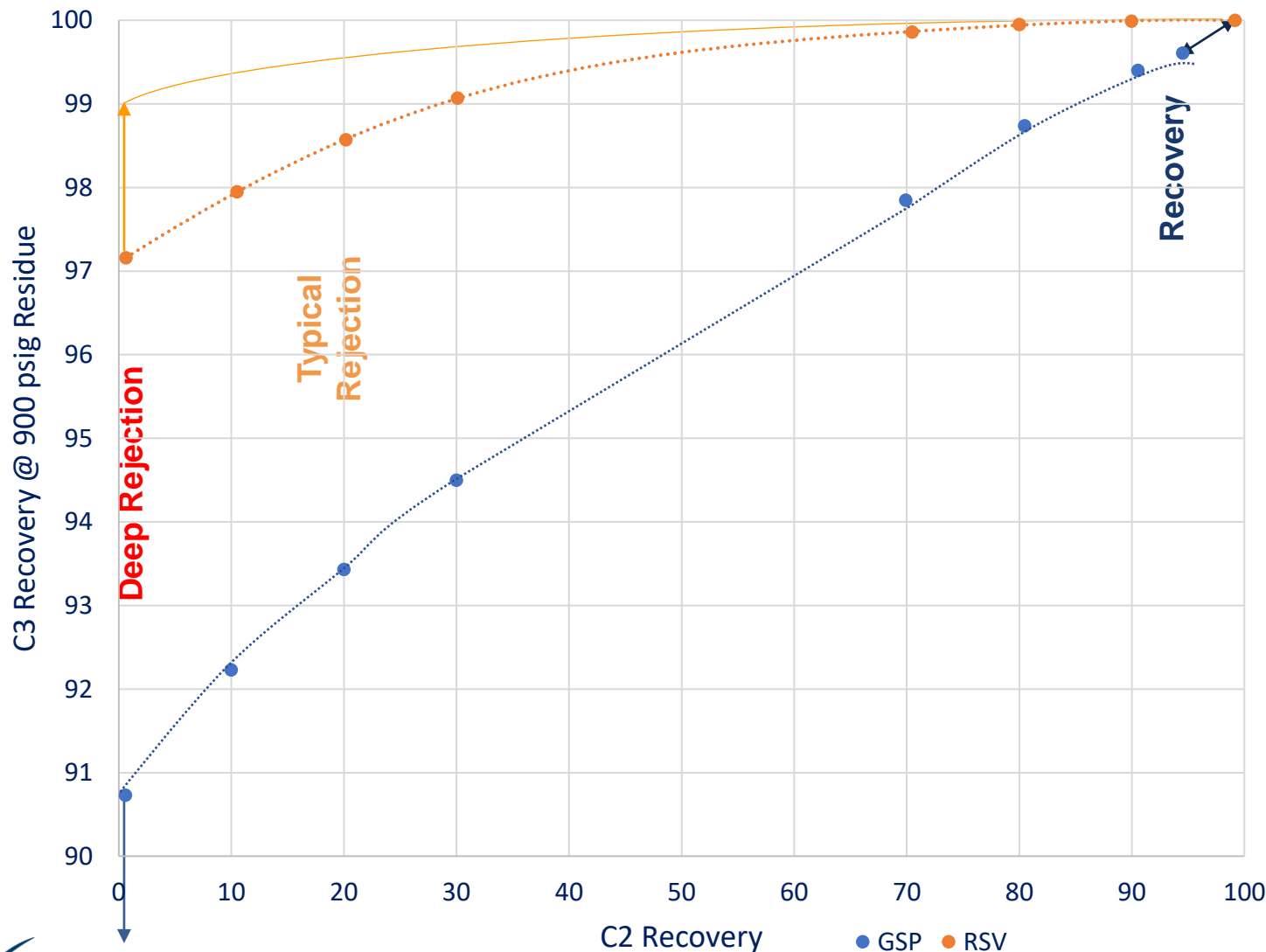
- Added reflux / tower pressure positively influences CO₂ freeze tolerance
- Although rejecting C₂ means rejecting CO₂, and therefore avoiding freeze, RSV plants have the following advantage:
 - ≥ 99% C₂ recovery at 1% CO₂ in comparison to GSP near 91%

Larger Backend

- Recompressor load ↑ = ↑ turbo frames or ↑ tower pressure / operating pressure / MAWP
- However, RSV in GSP mode has potential ↑ nameplate
 - For a fixed fee contract this could be \$6 million / year or more

GSP vs. RSV – The Reality in Recovery

GSP vs. RSV



Typical Narrative: RSV >> C₂%, however...

Rejection: GSP plants suffer losses in C₃ recovery.

- As rejection of C₂ deepens, ~10% C₃ is lost.

Additionally: as GPM ↑, Curve shifts ↓ ∴ C₃ ↓

- Energy of condensation for heavier HC streams.
- ↓ flows of residue; the cooling for inlet gas.

Residue Pressure Sensitivity:

- RSV plants perform differently from 900 to > 1,200 psig residue.
- C₃ recovery in deep rejection pivots from 97% to 99%.
- ↑ Residue pressure = ↑ C₃ Recovery.

Actual Performance:

- Based on integration of heat, the central recoveries around 30% to 60% C₂ may suffer a dip when switching from one mode to the other.

RSV: Equipment and Precautions

BAHX ALPEMA Temperature Swings, Cyclical Fatigue

- Typical: 28°C or 50°F max delta T
 - Frequent: 1°C or 1.8°F fluctuation.
 - Infrequent (startup / shutdown): 2°C/min or 3.8°F/min
- Suggest temperature probes on all sides of exchangers and to understand flow to each leg.
- Not necessarily worse than a GSP plant, ~ 20-year life, if maintained.

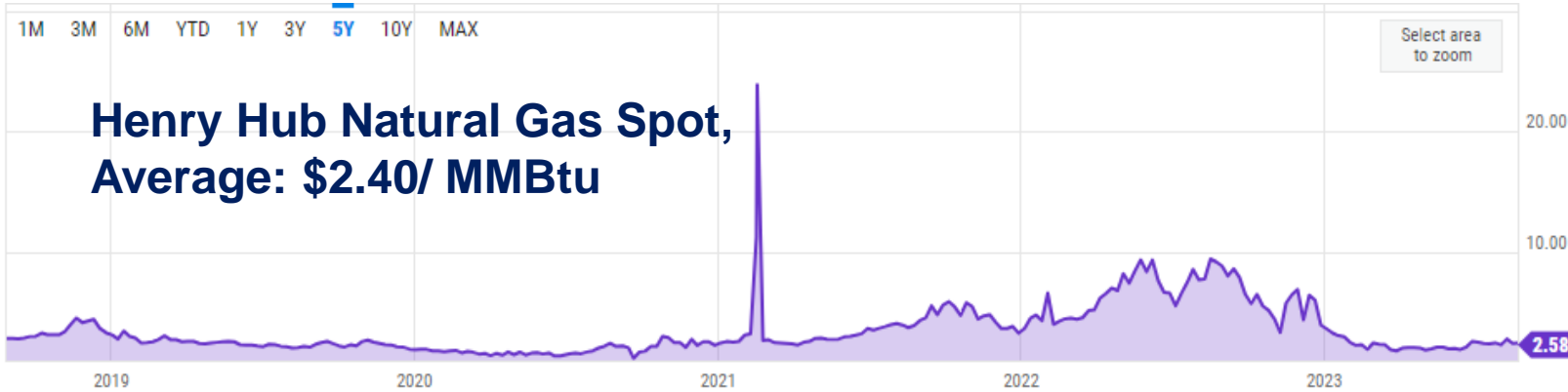
Filtration

- Aerosol residue oil is detrimental to BAHX performance. Failure = GSP style operation.
 - Cleaning is arduous.
 - Peco Facet “Natural Gas Pipeline Contaminant Removal Methods”
 - Transcend “The Impact of Aerosol Contamination on RSV Efficiency”
- Recommended: (1) Full residue stream filtration and (2) dedicated RSV slip stream filtration for aerosol.
- Delay RSV start-up until after compression break-in. Avoid pockets, be wary of slugs and ambient. Potential heat trace.
- Larger plants (~300MM+) with centrifugal recompression avoid this altogether.

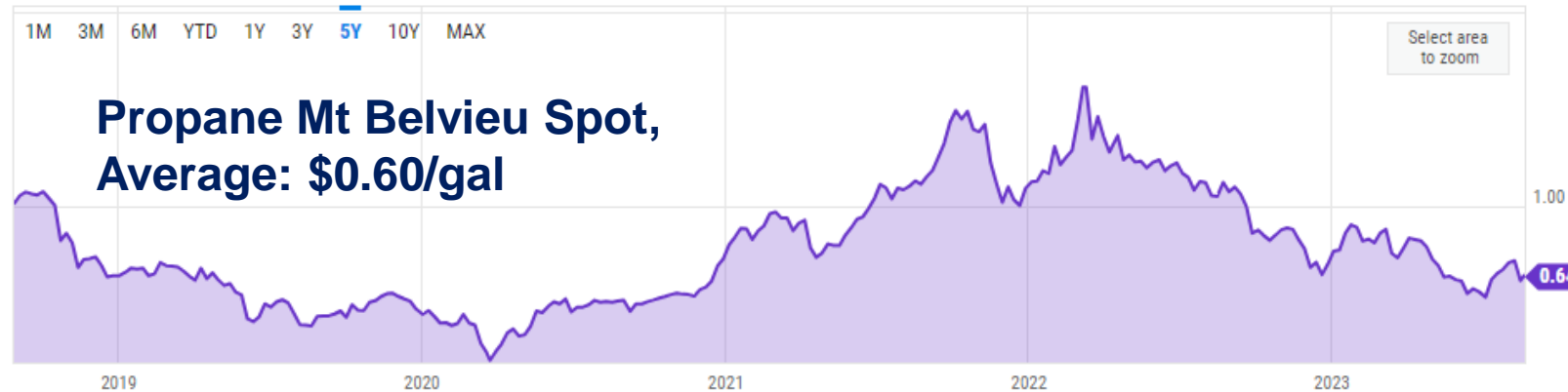
Tower

- Potential higher tower pressure = relative volatility and separation are worse ∴ ↑ HETPs / bed heights required.
- RSV bed physical properties already lead to higher HETPs. (Strigle, Packed Tower Design and Applications, EQ 9-1, 1987).
- Larger towers, when truck transport is difficult, may require shipment in pieces with field welds.

Commodities - Spot Price Averages



Ethane Mt Belvieu,
Average: \$0.24/gal



Butane Mt Belvieu Spot,
Average: \$0.93/gal

C₅⁺ Mt Belvieu Spot,
Average: \$1.31/gal

Utilities \$0.06/kWH, 1HP = 0.756kW
-\$0.10 on all liquids for transport and
fractionation

Plant Stats

- **7.2** GPM gas with **1.2** C₂/C₃ ratio
 - Higher Heating Value (HHV) match at 1,047
 - C₂ is not a valued liquid
 - From \$0.24 to \$0.31
 - Processor ↑ \$5.9 million/year

	230 MM	GSP		RSV		
C ₂ %	94.1%	25.5%	99.3%	94.0%	14.9%	
C ₃ %	99.6%	93.9%	100.0%	100.0%	98.9%	
C ₄ %	99.9%	98.8%	100.0%	100.0%	99.9%	
Revenue-Utility-Processing/year	291.6M	289.7M	290.7M	291.45M	295.6M	

C₂ @ \$0.31 in the \$\$\$

Contracts (Superior Pipeline, "Gas Processing 101" Aug 2016 Midcon GPA)

- **FF:** Fixed Fee (stable for processors), \$0.65 / mscf
- **Percent of Index:** ↑↑ risk / reward for processors
- **Percent of Proceeds (Gas + Liquids):** Mild R/R ~ >12% to meet FF
- **Percent of Liquids:** Medium R/R ~ >20% to meet FF

How do I monetize incremental propane?

Plant Stats

- 5 GPM gas with 2.6 C₂/C₃ ratio
 - Higher Heating Value (HHV) match at 1,073
 - Due to incremental C₃, deeper rejection is an option
- Processor ↑ \$2.7 million/year

	230 MM	GSP	RSV
C ₂ %		17.0%	11.3%
C ₃ %		91.8%	99.0%
C ₄ %		98.5%	100.0%
Revenue-Utility-Processing/Year		221.5M	224.2M

Contracts

- **FF:** Fixed Fee (stable for processors), \$0.65 / mscf
- **Percent of Index:** ↑↑ risk / reward for processors
- **Percent of Proceeds (Gas + Liquids):** Mild R/R ~ >16.2% to meet FF
- **Percent of Liquids:** Medium R/R ~ >39.5% to meet FF
- Percentage contracts require ↑ to match fixed fee, due to ↓ richness and ↑ C₂/C₃ ratio.

Monetization RSV Cost & ROI

Controlling the Narrative

The Cost:

- RSV modifications + residue compression + turnkey adders
 - ~ \$8 million+ assumed.

The Payback (ethane negative market):

- Fixed fee payback: 0.4 to 1.5 years with capacity upgrades, or...
- Without capacity upgrades with ROI < 5 years,
 - Processing fee ↑ by \$0.03/ mscf (\$0.65 to \$0.68 / mscf)
 - Get paid for incremental propane

Alternative:

- Kicker incentives for greater contract recoveries are sometimes part of fixed fee contracts, but more commonly from C₂ perspective.
- RSV Fixed Fee processor with kicker, considering both C₂ and C₃ gains, is better.
 - **A curve of rejection-based contract could maximize the kicker.**

Expectation versus Execution

7.2 GPM but... C_2/C_3 ratio increases from 1.23 to 2.65

- It's not leaner, it's just rich in the wrong places...
- Higher Heating Value (HHV) Issues = > C_2 required
 - Pivots RSV from 15% C_2 to 47% C_2 to hit < 1,080 HHV
 - *Benefit: Since RSV loses less C_3 , then deeper rejection can occur.*
 - *GSP is closer to 51% required recovery.*
 - *The revenue on gas and liquids is nearly identical.*
- Composition Limited: Volume of C_3+ is lower. Profitability is diminished.
 - Higher POL contracts required: ↑ to 29% to meet fixed fee rate of a 1.23 ratio gas.
 - Ask for 50% more liquids.

Conclusions

- Percentage of profit / liquid contracts are subject to C_2/C_3 sensitivity
 - If not varied based on C_2/C_3 ratio are subject to higher risk
- Fixed fee is unaffected, but the liquid volume is reduced by 23%
 - Kicker therefore is lower and ROI longer

C₂ in the Green: RSV was made for this

- Rejection recollection, due to HHV target of 1,047 HHV, the 7.2 GPM gas performs as follows →
- Recovery
 - Economics are per previous 94% GSP, 99% RSV
 - Most GSP plants are going to only see 90% to 92%
 - Ethane economics pivot, and highest percentage recovery is not always best.
 - Incremental ethane doesn't always add up the way incremental propane does.

<u>230 MM</u>	GSP	RSV
C ₂ %	25.5%	14.9%
C ₃ %	93.9%	98.9%

	September 2018	July 2020	June 2022	May 2023	July 2023
Nat Gas (\$/MMBTU)	\$ 3.00	\$ 1.72	\$ 7.67	\$ 2.15	\$ 2.55
Ethane (\$/MMBTU)	\$ 7.95	\$ 3.23	\$ 9.67	\$ 3.07	\$ 4.80
Adjusted Ethane (T&F) (\$/MMBTU)	\$ 6.44	\$ 1.72	\$ 8.16	\$ 1.56	\$ 3.29
RSV vs GSP Rejection	3.4M\$	3.2M\$	9.4M\$	7.5M\$	3.5M\$
RSV vs GSP Recovery	3.2M\$	0.1M\$	0.7M\$	-0.1M\$	0.8M\$
Suggested Operation	RSV Rec	RSV Rej	RSV Rec	RSV Rej	RSV Rec
Rec vs Rej RSV	44.2M\$	-0.7M\$	3.4M\$	-8.6M\$	8.7M\$

*\$0.10/gal transport + fractionation
~\$1.51/MMBTU

*Rejection +21.5 GPM C₃

<https://www.eia.gov/energyexplained/hydrocarbon-gas-liquids/prices-for-hydrocarbon-gas-liquids.php>

Conclusions and Findings

RSV plants > C₃ recovery across all performance modes.

RSV has a quick ROI of 2 to 5 years even in a C₂ negative market.

Alternatively, a larger nameplate can help pay for the process in less than 1 to 2 years.

RSV Rejection economics for 230MM can yield \$3 million to \$9 million / year in C₃ revenue; depending on richness, level of rejection, and C₂/C₃ ratio.

GPM alone is not enough to define POP or POL contracts, C₂ / C₃ ratio is key.

RSV in a GSP mode, may have higher nameplate.

C₃ stability is key for profitability and should make its way into contracts.

A plant that pivots between a focus on nameplate, C₂ recovery, and C₃ stability is more flexible; therefore, desirable than classic GSP.

Questions?

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Thank You

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